

TOMSK POLYTECHNIC UNIVERSITY FACULTY OF MECHANICAL ENGINEERING

## **UNDERGRADUATE THESIS**

### HIGH PRESSURE EJECTION SYSTEM OF DREDGING

BY

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## INTRODUCTION

### **REQUIREMENTS OF UNDERGRADUATE THESIS**

1. TO DETERMINE THE METHODOLOGY OF CALCULATING THE HYDRAULIC PARAMETERS OF A DREDGER.

2. TO DESIGN A PRODUCTION PROCESS FOR THE MANUFACTURE OF A DRIVING SHAFT (COMPONENT PART OF THE DREDGER).

### **INITIAL DATA**

DREDGING DEPTH.	1m 5m
MAXIMUM DISTANCE BETWEEN PONTOON AND	
DISCHARGE POINT.	120m
PRODUCTIVITY.	15m <sup>3</sup> /hr
DESIGN DRAWING OF DRIVING SHAFT	GIVEN
MINIMUM THICKNESS OF SAND LAYER	0.5m
DESIRED RANGE OF SAND GRAINS	0.062.1mm



#### FIG.1 -DISTRIBUTION OF SAND AND GRAINS OF SAND UNDER WATER QUANTITY

D1=D2 , Vs2>>Vs1 where: 1-water ,2-sand layer ,3-land above water level ,Vs1- volume of sand close to riverbank ,Vs2- volume of sand at a distance L1 from the river bank.



### FIG.2 - LAYOUT OF COMPACT SAND DREDGER

Where 1-discharged sand, 2- Hopper ,3-discharge pipe ,4-onboard suction pump ,5 onboard water-injector pump ,6-pontoon /barge, 7-water injection pipe ,8-suction pipe ,9-sand layer ,



SUCTION LINE

## SAND VELOCITY EXPERIMENT

### **GRAPH OF TIME AGAINST SAND GRAINS**

#### GRAPH OF VELOCITY AGAINST SAND GRAINS DIAMETER



### RESULTS

### **SUCTION LINE**

 $v_{sandgrain} = k_v \times D_{sandgrain} = 0.068 \times 2.1 = 0.143 [\frac{m/s}{mm} \times mm] = 0.143 m/s$ 

V=0.3m/s; D= 0.133m; Δp<sub>Σ</sub> =0.03MPa

### **DISCHARGE LINE**

### **V=2.5 m/s; D=0.05m;** Δp<sub>Σ</sub> =0.4MPa

$$N_{P(D=50mm)} = 2.8Kwatts$$

# **CENTRIFUGAL PUMP**



### **EJECTOR PUMP**

The design is quite simple; an ejector is a pumping device. It has no moving parts. Rather, it uses a fluid or gas as a motive force. Very often, the motive fluid is steam and the device is called a "steam jet ejector." Basic ejector components are the steam chest, nozzle, suction, throat, diffuser and the discharge





FIG.4.5 PARTS OF EJECTOR PUMP FOR DREDGING

# **EJECTOR PUMP SPECIFICATIONS**



- D<sub>2</sub>=50mm- discharge pipe diameter from previous calculations;
- H<sub>3</sub>=(2...5)D<sub>THROAT</sub>-from hydraulic engineer's manual;
- H<sub>2</sub>=(2...5)D<sub>NOZZLE</sub>-from hydraulic engineer's manual;
- H<sub>1</sub>=(0.8...3)D<sub>NOZZLE</sub>-from hydraulic engineer's manual;
- These conditions are required to be met in throat depending on the kind of pressure needed in the diverging discharge line.
- The converging-diverging angles are within the range of (5.....15) degrees  $\frac{Area_{throat}}{Area_{mottive-fluid-nozzle}} \ge 4; high-pressure$

$$\frac{Area_{throat}}{Area_{motive-fluid-nozzle}} < 4; low-pressure$$

For an ejector pump, the discharge flow rate  $(Q_2)$  is the sum of the motive fluid's flow rate the inlet fluid's flow rate: where the motive fluid constitutes 20% of the total flow rate and the inlet fluid accounts for the remaining 80%.

 $Q_2 = Q_0 + Q_1 \implies Q_0 = 0.2Q_2 = 0.2 \times 0.0042 = 0.00084m^3 / s$  $P_0 = (P_0 - P_2) + \Delta P_{\Sigma} \qquad (P_0 - P_2) = \Delta P_0$ 

 $\Rightarrow \Delta P_0 = \rho_0 gh$ 

## **COMPARISON OF CENTRIFUGAL AND EJECTOR PUMP**

CHARACTERISTICS	CENTRIFUGAL PUMP	EJECTORPUMP
Discharge diameter	50mm	50mm
Discharge velocity	2.5m/s	2.5m/s
Suction velocity	0.3m/s	
Total pressure loss	0.4MPa	0.4MPa
Pump power	1.67Kwatts	1.64Kwatts
Construction	Very hard	Quite simple
Cavitation	Certain	Practically no
Vane/bearing damage	yes	no
Shaft breakage	yes	no
Rotating parts	yes	no

### CONCLUSION

Based on the content of the table above we conclude that the ejector pump is preferable to centrifugal pump in the design of a mini dredger.



3. CENTRE HOLE ON LEFT SIDE OF SHAFT IS ALLOWED.



**GRADUATE WORK.TAMP.TME.54.2** GRADUATE WORK. TECHNOLOGY OF AUTOMATED MANUFACTURINGAND PRODUCTION. LECHNOLOGY OF MECHANICAL ENGINEERING. ΛИТ MASS SCALE DOC. NO SIGN, DATE SHAFT PRODUCTION 1:1 4/03/0 DESIGNER KA, DIGITEMIET DRAWING CHECKED BY NO PAGES: 2 -. KOZLOV V.N AGE NO: 2 TOMSK POLYTECHNICAL UNIVERSITY. DESIGN AND PRODUCTION FACULTY. STUDY GROUP:154A4A STEEL 40X GOST 2.801-74









