Unit 13. Alkylation. Exercises

Read the description of alkylation mechanism stages Complete the alkylation mechanism with the name of each stage.

Alkylation is one of the classic examples of a reaction or reactions proceeding via the **carbenium ion mechanism**. These reactions include an **initiation step** and a **propagation step** and may include an **isomerization step**. In addition, **polymerization**, **cracking steps** and **hydrogen transfer** may be involved. However, these side reactions are generally undesirable.

Isomerization

Isomerization is very important in producing good octane quality from a feed that is high in 1-butene. The isomerization of 1-butene is favored by thermodynamic equilibrium. Allowing 1-butene to isomerizes to 2-butene reduces the production of dimethylhexanes and increases the production of trimethylpentanes.

Hydrogen transfer

The hydrogen transfer reaction is most pronounced with propylene feed. The reaction also proceeds via the carbenium ion mechanism. In the first reaction, propylene reacts with isobutane to produce butylene and propane. The butylene is then alkylated with isobutane to form trimethylpentane.

Cracking disproportion

The larger polymer cations are susceptible to cracking or disproportionation reactions, which form fragments of various molecular weights. These fragments can then undergo further alkylation.

Initiation

The initiation step (generates the tertiary butyl cations that will subsequently carry on the alkylation reaction.

Overall reaction

From the viewpoint of octane, this reaction can be desirable because trimethylpentane has substantially higher octane than the dimethylpentane normally formed from propylene. However, two molecules of isobutane are required for each molecule of alkylate, and so this reaction may be undesirable from an economic viewpoint.

Propagation

Propagation reactions involve the tertiary butyl cation reacting with an olefin to form a larger carbenium ion, which then abstracts a hydride from an isobutane molecule. The hydride abstraction generates the isoparaffin plus a new tertiary butyl cation to carry on the reaction chain.

Polymerization

The polymerization reaction results in the production of heavier paraffins, which are undesirable because they reduce alkylate octane and increase alkylate endpoint. Minimization of this reaction is achieved by proper choice of reaction conditions.

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Alkylation mechanism.

1)
$$C = C-C + HF \longrightarrow C-C-C \longrightarrow C-C-C \xrightarrow{iC_4} C-C-C + C-C-C \xrightarrow{i} C$$

- Match the type of alkylation process with its description.
- 1) Alkylation without catalyst
- 3) Alkylation in presence of hydrofluoric acid
- 2) Alkylation in presence of sulphuric acid 4) Alkylation in presence of zeolite catalyst
- A Process has no mechanical stirring. The catalyst of this process is a very hazardous material for humans because it can penetrate and damage tissue and bone. This type of process is less favourable because of the mitigation of acid catalyst vapour.
- C Alkylation between isobutane and olefin must be run under severe conditions such as T = 500 °C and P = 20-40 MPa.
- 1).....; 2).....; 3).....; 4)......

- In this process multiple reactors are used to allow for the catalyst regeneration cycle. This process is considered as less harmful for equipment, environment and people's health because of the fact that catalyst is not corrosive and does not vaporize.
- The contactor reactor is used in this type of alkylation technology as one of the technology configuration. Another configuration of this process represents a train of reactors with mixing devices.

Fill in the gaps with suitable words from the list. Alkylate

| branched hydrocarbons | isostrinner tower | |
|---|-------------------------|--|
| isostripper tower | tube bundle | low temperature conditions |
| acid strength | FCC unit | feed for the alkylation unit |
| emulsion | sulfuric acid | isobutylene with isobutane |
| product, normal butane as side of | lraw, and alkylate as l | pottom product. |
| | | to remove isobutene as overhea |
| | _ | |
| • • | | taline water stream. The treated contractor |
| acid is charged to the reactor. The impure alkylate stream | m contain some esters | s, which are removed by reacting with fres |
| | it acid is withdrawn a | nd an equivalent amount of 98.5 wt % fres |
| | | ed 9) (90 wt 9 |
| | | ount of acid is consumed as a result of sid |
| | | for the alkylation reaction and theoreticall |
| - | • | lsion pump between the reactor and settler. |
| | | o the bottom and is returned to the suctio |
| - | | an acid settler where acid and hydrocarbo |
| | | s withdrawn from the contractor on th |
| | | by the impeller at high rates within th |
| | | erses hydrocarbon feed into the acid catalys |
| • • | • | ected into the suction side of the impelle |
| | | to remove hea |
| | - | r are horizontal pressure vessels containin |
| range. Alkylate has an RON of | | |
| | | in the gasoline boilin |
| allzuloto product is a minter- | Ine | process is carried out at 7 to 10 °C. The |
| | | s and highly exothermic and is favored by |
| isobutane separated from field b | | a and highly avadagmais and in face. |
| • | · | the olefin. So provision is made to suppl |
| | | ase the MTBE unit is shut down, feed to the |
| | _ | ISO butylene and isobutane become |
| • | | nainly depletes isobutylene from this feed |
| | | d lighter constituents. The bottom from th |
| | | FCC gases ar |
| hydrofluoric acid (HF) catalyst. | | 700 |
| | | n the presence of sulfuric acid (H_2SO_4) of |
| | | manufactured by the reaction of |
| • | _ | viation gasoline blend stock because of it |
| | | |